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ABSTRACT

MATHEMATICAL MODELLING AND IMMEDIATE AND LATENT QUALITY OF NATURAL IMMATURE COFFEE UNDER DIFFERENT DRYING CONDITIONS

Ednilton T. de Andrade¹, Isabella A. Lemos¹, Camila de A. Dias¹, Paula de A. Rios^{1*}, Flávio M. Borém¹

^{1*}Corresponding author. Universidade Federal de Lavras/ Lavras - MG, Brasil. E-mail: paulariosagricola@gmail.com | ORCID ID: https://orcid.org/0000-0002-2836-918X

KEYWORDS

Drying kinetics, *Coffea arabica* L., post harvest.

This work aimed to study the immediate and latent effects of different relative humidities on the quality of dried coffee fruits, describe the drying kinetics of natural immature coffee (*Coffea arabica* L.), and evaluate the mathematical model that best fits the experimental drying data. The drying was carried out in a fixed layer dryer coupled to a composite air conditioning system in which the drying air was controlled with an air flow of 20 m³.min¹.m⁻², at a temperature of 40 °C, and at relative humidities of 10%, 17.5% and 32.5%. Manually harvested coffee fruits were used and dried to a mean water content of 0.120 dry basis (d.b). After drying, the kinetic curve and the physical and physiological properties were determined. The coffee was stored in permeable packs for 6 months. The electrical conductivity, potassium leaching, and colour analysis were performed every 2 months. For the modelling adjustment, the models were tested, and the Midilli model had the best fit with the drying kinetics of the immature coffee. No immediate damage was observed in the physical and physiological quality of the coffees, and latent damage was perceived after 120 days of storage for the natural immature coffees.

INTRODUCTION

Strip harvesting is the predominant coffee harvesting method in Brazil, and it yields a very heterogeneous product consisting of ripe (cherry), unripe (green) and overripe (raisins and dried-on-trees) berries; foreign materials; and impurities (Borém, 2014). Additionally, coffee has a high water content at the time of harvest compared to other grains (Botelho et al., 2016). Therefore, drying is a critically important post-harvest step and should be started soon after harvesting to quickly reduce the high water content of the berries and prevent fermentation, which may impair coffee quality (Resende et al., 2009).

After harvest, the coffee is processed. In the dry processing, the berries are dried whole, resulting in natural coffee, whereas wet processing results in parchment coffees, with the peel, pulp, and mucilaginous material removed. During the wet processing stage, ripe berries are separated from unripe berries by peeling, with the ripe berries being peeled, and the whole unripe berries being directed down a different path, thus generating two different coffee portions (Borém, 2008). Additionally, according to Borém (2014), the coffee processing stage also aims to separate the berries into more homogeneous lots. The

The preservation of bean quality during drying is based on the premise that reducing the amount of available water leads to a reduction in water activity and, consequently, in the speed of chemical and biochemical reactions, as well as the development of microorganisms, allowing safe storage for longer periods (Araujo et al., 2014). Dry processed coffees are more sensitive to drying at high temperatures than wet processed coffees, resulting in lower physiological performance (Alves et al., 2017).

An alternative for increasing the drying rate without causing thermal damage to the beans is to reduce the relative humidity of the drying air by other means, such as by circulating the air through a desiccant that adsorbs

berries may be separated by maturation stage, water content, size and density, among other factors, which facilitate subsequent operations, especially drying and thereby avoiding possible compromises in the quality of the beverage. For coffee drying, the currently available technology allows increasing the drying rate by increasing the temperature, the airflow or by decreasing the relative humidity. The development of technologies or methodologies that provide rapid dehydration without the use of high drying temperatures is a highly promising alternative, especially for the reduction of processing time.

¹ Universidade Federal de Lavras/ Lavras - MG, Brasil. Received in: 9-11-2018 Accepted in: 2-14-2019

and removes moisture from the drying air or by reducing the air dew point temperature (Ondier et al., 2010; Isquierdo et al., 2013).

To simulate the coffee drying process, whose principle is based on the drying of successive thin layers of the product, a mathematical model that satisfactorily represents the water loss is used (Giner & Mascheroni, 2002). Thin-layer drying of agricultural products allows the drying rates of the product to be determined by collecting data on the mass losses that occur in a sample during the water removal (Monte et al., 2008). Thus, thin-layer drying curves vary according to the species, variety, environmental conditions and postharvest preparation method, among other factors.

Most coffee goes through a period of storage until it is marketed, and therefore, the storage conditions can change its physical, chemical and sensory characteristics (Oliveira et al., 2015). Damages caused by drying may arise in a latent manner, causing changes in coffee quality.

Different analyses are used as indicators of coffee quality by providing information on the physical and physiological state of the product and promoting an understanding of the phenomena and/or changes that occur in beans subjected to different postharvest processes. Previous studies have correlated the maintenance of physiological quality during this process with the sensory quality of the beverage (Borém et al. 2014; Oliveira et al., 2015; Alves et al., 2017).

The colour of immature coffee beans may be related to the quality of the beverage and is an important factor for the valorisation of the product. Changes in colour are strong indicators that oxidative processes and enzymatic biochemical transformations that alter the composition of the precursors responsible for the flavour and aroma of the beverage have occurred, thereby resulting in decreased quality (Borém et al., 2013; Rendón et al., 2014; Abreu et al., 2015).

The paucity of studies on the drying of immature coffee, which shows heterogeneity of the maturation stages when harvested, increases the importance of theoretical research on the drying process of agricultural products; therefore, the objective of this study was to obtaining the drying curves of unripe coffee berries (*Coffea arabica* L.) using mathematical models. A secondary objective was to determine the immediate and latent effects of different relative humidities during drying on the quality of the coffee berries.

MATERIAL AND METHODS

The present study was conducted at the Agricultural Products Processing Laboratory, Department of Engineering, Federal University of Lavras (Universidade Federal de Lavras - UFLA). The experiment used unripe coffee beans (*Coffea arabica* L. cv. Catuaí Vermelho IAC 99) selectively harvested in a commercial plantation of the Três Porteiras property, located in the municipality of Ingaí, Minas Gerais, Brazil. All harvesting and processing procedures were performed according to Borém (2014). A fixed-bed dryer coupled to an air conditioning system was used for drying, and a drying air temperature of 40 °C was adopted. The air characteristics were controlled by a Laboratory Air Conditioning System (LACS) model proposed by Fortes et al. (2006). This equipment allows the flow rate (20 m³.min⁻¹.m⁻²), temperature (T) and relative humidity (RH) of the air to be accurately controlled during drying. Three relative humidity values were tested: $10 \pm 2\%$, $17.5 \pm 2\%$ and $32.5 \pm 2\%$. The air flow was regulated by a frequency inverter (Weg, model CFW-10).

The dew point temperature was measured inside the LACS chamber, and the drying air temperature was measured in the plenum chamber, under the perforated bottom trays, by thermocouples connected to universal controllers (Novus, model N1100). The relative humidity of the drying air was measured by a portable digital thermo-hygrometer (Instrutemp, model ITLOG 80) with a sensor inserted inside the plenum chamber. The temperature of the drying air around the coffee berries was measured with mercury thermometers placed at the centre of the sample.

Drying was monitored by the gravimetric method (mass loss) until the desired water content was reached. The trays containing the product were periodically removed from the chamber at half-hour intervals in the first 5 hours and then hourly until the end of the process. An analytical balance (Shimadzu, model UX420H) with a resolution of 0.01 g was used for weighing, according to the equation below.

$$Ut = \frac{Wwi - (Wti - Wtt)}{Wdm}$$
(1)

Where:

Ut is the water content (kg water.kg dry matter⁻¹) (dry basis, db) at time t;

Ww_i is the initial water weight (kg);

Wt_i is the initial total weight (kg);

Wt_t is the total weight at time t (kg), and

W_{dm} is the dry matter weight (kg).

In the analysis of the drying data, the moisture ratio (MR) is essential to describe different thin-layer drying models. The MR during drying as a function of the evaluated variables was determined by [eq. (2)]. For all tested conditions, the MR values as a function of drying time were fitted to models used to describe the drying kinetics of the coffee (Table 1).

$$MR = \frac{U - Ue}{Ui - Ue}$$
(2)

Where:

MR is the moisture ratio (dimensionless);

U is the water content of the product (db) at time t;

 U_e is the equilibrium water content of the product (db), and

U_i is the initial water content of the product (db).

TABLE 1.	Mathematical	models	used to	predict	drving	kinetics

Model designation	Model	Equation	
Two-term	$MR = a \cdot exp(-k_0 \cdot t)$	$+b \cdot \exp(-k_1 \cdot t)$	(3)
Two-term exponential	$MR = a \cdot exp(-k \cdot t)$	+ (1-a) exp (-k \cdot a \cdot t)	(4)
Modified Henderson & Pabis	$MR = a \cdot exp(-k \cdot t)$	$+b \cdot exp(-k_0 \cdot t) + c \cdot exp(-k_1 \cdot t)$	(5)
Henderson & Pabis	$MR = a \cdot exp(-k \cdot t)$)	(6)
Midilli	$MR = a \cdot exp(-k \cdot t)$	n) + b · t	(7)
Newton	$MR = \exp(-k \cdot T)$		(8)
Page	$MR = \exp(-k \cdot T^{n})$)	(9)
Thompson	$MR = \exp\{[-a - (-a^2)]$	$+ 4 \cdot b \cdot t)^{0.5}] \cdot (2 \cdot b)^{-1}$	(10)
Verma	$MR = -a \cdot exp(-k \cdot t)$	$(1-a) \exp(-k_1 \cdot t)$	(11)
Wang and Sing	$MR = 1 + a \cdot t + b \cdot t$	t^2	(12)
Valcam	$MR = a + b \cdot t + c \cdot t$	$t^{1,5} + d \cdot t^2$	(13)

MR: moisture ratio; t: drying time (h); k, k₀ and k₁: drying constants; a, b, c, d, n: model coefficients.

To fit the mathematical models, nonlinear regression analyses were performed using the Gauss-Newton method in the software STATISTICA $5.0^{\text{(B)}}$ (Statsoft, Tulsa, USA). The best model was selected based on the following statistical parameters: standard deviation of the estimate (SE), mean relative error (P), and coefficient of determination (R²). The standard deviation of the estimate and the mean relative error were calculated using eqs (14) and (15), respectively.

$$SE = \sqrt{\frac{\Sigma (Y - \hat{Y})^2}{DF}}$$
(14)

$$P = \left[\left(\frac{100}{n} \right) \Sigma \left(\frac{\left| Y - \hat{Y} - \hat{Y} \right|}{Y} \right) \right]$$
(15)

Where:

SE is the standard deviation of the estimate (decimal);

Y is the experimentally observed value;

 \hat{Y} is the value calculated by the model;

DF is the degrees of freedom of the model (number of model parameters -1);

P is the mean relative error (%), and

n is the number of observed datapoints.

To characterize the coffee quality, the physical and physiological properties of the coffee were determined after drying and then every 2 months during the 6 months of storage.

Colour quantification was performed using a colourimeter (Minolta CR-410) previously calibrated on a white surface according to pre-established standards (Bible & Singha, 1993). Measurements were performed directly on

the beans, which were placed on a glass Petri dish so that the beans covered the entire surface on which the readings were taken, maintaining their integrity.

The electrical conductivity of the raw beans was determined according to the method proposed by Krzyzanowski et al., (1991). For this purpose, two replicates of 50 grains of each sample were weighed at 0.001 g precision and immersed in 75 mL of distilled water inside 200-mL plastic cups. Then, these containers were placed for 5 h in a forced-air biochemical oxygen demand chamber (Quimis, model Q-315D) regulated to 25 °C, after which time the electrical conductivity of the imbibition water was read using a benchtop conductivity meter (BEL, model W12D). After the readings were obtained, the electrical conductivity was calculated using [eq. (16)], and the results were expressed in μ S.cm⁻¹.g⁻¹ of grains.

$$CE = \frac{CE'}{Weight (g)}$$
(16)

Where:

CE' is the electrical conductivity reading (μ S.cm⁻¹).

The leaching of potassium ions was measured in the raw beans after the electrical conductivity reading, and the same solutions were subjected to determination of the amount of leached potassium. The reading was performed in a flame photometer (Digimed, Model NK-2002). With the data obtained, the amount of leached potassium was calculated according to [eq. (17)], and the results were expressed in parts per million (ppm).

$$LK = \frac{(LK' \times Dilution \times 1.56)}{Weight (g)}$$
(17)

Where:

LK' is the potassium leaching reading (ppm).

The percentage of black-green defective beans in the raw bean samples was determined. From a sample of natural unripe coffee processed manually, 100 beans were counted and separated into immature and black-green defective beans, with percentages being directly obtained.

The experiment was set up in a 3x1x4 factorial arrangement (three drying relative humidities), one coffee type (natural immature) and four storage times in a completely randomized design, with four replications per drying treatment, corresponding to each of the dryer trays. The airflow rate adopted was 20 m³.min¹.m⁻², with an air

temperature 40 °C and relative humidities of $10 \pm 2\%$, 17.5 $\pm 2\%$ and $32.5 \pm 2\%$. The coffee was stored for 6 months, with physiological assessments performed every 2 months.

RESULTS AND DISCUSSION

Table 2 shows the values of the statistical parameters coefficient of determination (R^2), mean relative error (P) and standard deviation of the estimate (SE) used to compare the eleven analysed drying models under the three tested immature coffee drying conditions.

TABLE 2. Coefficient of determination (R^2 , %), mean relative error (P, %) and standard deviation of the estimate (SE, decimal) values obtained for the analysed models describing the drying kinetics of natural immature coffee under different relative humidity.

Model	R ²	Р	SE	R ²	Р	SE	R ²	Р	SE
		RH=10%)	-	RH=17.5%	ý 0]	RH=32.5%	6
Two-term	99.84	1.015	0.146	99.38	2.439	0.355	99.69	1.426	0.275
Modified Henderson & Pabis	99.84	1.015	0.113	99.38	2.441	0.275	99.69	1.443	0.215
Henderson & Pabis	99.84	1.015	0.253	99.38	2.438	0.614	99.69	1.426	0.476
Midilli	99.96	0.014	0.002	99.97	0.000	0.000	99.99	0.004	0.001
Newton	99.78	0.508	0.127	99.29	1.708	0.430	99.61	0.863	0.288
Page	99.94	0.510	0.127	99.79	1.798	0.453	99.92	0.848	0.283
Thompson	99.95	0.023	0.006	99.95	0.358	0.090	99.98	0.050	0.017
Verma	99.92	0.340	0.060	99.82	0.341	0.061	99.67	1.369	0.323
Wang and Sing	98.99	2.331	0.581	99.34	2.255	0.568	99.16	1.946	0.649
Valcam	99.91	0.000	0.000	99.93	0.000	0.000	99.94	0.000	0.000
Two-term exponential	99.78	0.602	0.150	99.29	1.754	0.442	99.24	1.201	0.401
Diffusion approximation	99.94	0.398	0.070	99.83	1.559	0.278	99.91	0.830	0.196

All fitted models had satisfactory coefficients of determination ($R^2 > 90\%$) and mean relative error below 10%, indicating that these models are suitable for representing the studied phenomenon (Mohapatra & Rao, 2005). According to Kashaninejad et al. (2007), the mean relative error values indicate deviation of the observed values relative to the curve estimated by the model. Thus, together with this statistical parameter, the goodness-of-fit of the model was adapted as an additional criterion to all studied relative humidities during drying.

Thus, based on all statistical parameters used, the model chosen to represent the natural immature coffee drying phenomenon for all relative humidities studied was the Midilli model. The R² was greater than 99.9%, and the SE values were less than 0.05 for all studied relative humidities.

This model was also used by Coradi et al., (2017) to describe the drying of de-pulped coffee. Corrêa et al. (2010) also recommended the Midilli mathematical model to describe the drying kinetics of coffee berries because of the satisfactory fit obtained. The Midilli model also showed satisfactory fit to the drying data of several other agricultural products, such as strawberry (Sousa et al., 2014), cowpea (Camicia et al., 2015) and garlic (Cagnin et al. 2017). In addition to being an internationally recognized model, the Midilli model is mathematically more practical, presenting a smaller number of parameters, making its application and use simpler in drying simulations.

Table 3 shows the coefficients of the mathematical model chosen based on the statistical selection criteria in the modelling of drying curves for natural immature coffee at the relative humidities of 10%, 17.5% and 32.5%.

TABLE 3. Coefficients of the mathematical model chosen based on the statistical selection criteria fitted to the drying curve of natural coffee for the three relative humidities studied.

Model	DU (0/)	Coefficients				
	КП (70) —	a	k	n	b	
Midilli	10	0.997120	0.031255	1.045390	-0.000232	
	17.5	0.977648	0.023759	1.109212	-0.000467	
	32.5	0.989149	0.023013	1.079989	-0.000262	

As shown in Table 3, the drying constant 'k' is higher for the relative humidity of 10% when compared to the relative humidity of 32.5%. This finding, which is easily observed in Figure 1, is expected because lower relative humidity leads to a higher drying rate, with the equilibrium water content being achieved in less exposure time for the product to the drying air.

Figure 1 shows the behaviour of the moisture ratio observed and estimated by the Midilli model for immature

coffee at the relative humidities of 10%, 17.5% and 32.5% during drying.

As expected, when berries were dried in high relative humidity of 32.5%, 75 hours of drying were required, which was longer than required under the drying air condition with lower relative humidity of 10%, which required 62.5 hours. The values estimated by the Midilli model showed satisfactory representation, with sufficient fidelity in the description of the drying behaviour.



FIGURE 1. Moisture ratio values of observed and estimated by the Midilli model for drying natural immature coffee at the relative humidity of 10%, 17.5% and 32.5% as a function of time.

Figures 2, 3 and 4 show the behaviour of the drying kinetics at 40 °C and relative humidity of 10%, 17.5% and 32.5%, respectively, as well as the behaviour of the water reduction rate under each condition.



FIGURE 2. Moisture ratio values observed and estimated by the Midilli model and water reduction rate for natural immature coffee drying at 10% relative humidity and temperature of 40 °C as a function of time.



FIGURE 3. Moisture ratio values observed and estimated by the Midilli model and water reduction rate for natural immature coffee drying at 17.5% relative humidity and temperature of 40 °C as a function of time.



MR observed — MR simulated — Water Reduction Rate

FIGURE 4. Moisture ratio values observed and estimated by the Midilli model and water reduction rate for natural immature coffee drying at 32.5% relative humidity and temperature of 40 °C as a function of time.

Under all drying conditions, the initial water reduction rate was higher, which occurs because the capillary and solvent water are freer in the bean and are more easily removed during drying. Table 4 shows the mean values of the potassium leaching test of natural immature coffee for the interaction of the factors of relative humidity during drying and the storage time.

TABLE 4. Mean potassium leaching (LK) values of natural immature coffee for the interaction of the relative humidity during drying and the storage time factors.

Coffee type	Storage time (days)	Relative humidity (%)				
		10	17.5	32.5		
Natural immature	0	409.285 Aa	406.189 Aa	422.022 Aa		
	60	797.316 Bb	722.092 Bb	581.082 Ab		
	120	938.825 Bc	687.364 Ab	660.606 Ac		
	180	916.769 Ac	887.331 Ac	805.852 Ad		

Means followed by the same uppercase letter in the rows and lowercase letters in the columns do not differ significantly at the 5% probability level by the Scott-Knott test.

The potassium leaching values varied during storage, and the longer the storage time was, the higher the values obtained. That is, the coffee suffered physiological damage during storage. The potassium leaching values were influenced by the effect of the relative humidity during drying on the storage times, and in general, the highest potassium leaching values were found in natural immature coffee beans dried at a relative humidity of 10%. This finding suggests that the lower the relative humidity used, i.e., the faster drying, the greater the cellular damage to the coffee because this test is indicative of cellular disorganization (Malta et al., 2013). Immature coffee has thinner cell walls due to the low cellulose content, which is accompanied by greater loss of permeability control and solute leakage. As in the present study, Isquierdo et al. (2011) found that the lower the relative humidity is during drying, the greater the damage is to the cell membranes of natural coffee. Notably, the compounds of immature coffees

are not yet fully formed and thus can experience more intense damage, leading to membrane disorganization during the drying processes when the drying rate is higher and water evaporates more quickly, causing greater potassium leaching.

The evolution of the colour of immature coffee was another parameter used to characterize quality. The mean values of the L* and b* coordinates of the beans obtained from natural immature coffee according to the relative humidity of the drying air are shown in Table 5, which indicates the influence of this factor on the colour of the product. Values of the a* coordinate were not included, as they showed no significant trend. In general, an increase in the L* and b* coordinate values is observed when the relative humidity during drying is 32.5%, suggesting that in the slower drying processes, the beans have higher luminosity and decreased bluish tone, characteristics desirable for coffee beans.

TABLE 5. Mean L* and b* coordinate values for beans from natural immature coffee subjected to different drying conditions and stored for 180 days.

Coffee type	Relative humidity (%)	Drying time (hours)	L* coordinate	b* coordinate
	10	81.3	31.063 a	17.596 a
Natural immature	17.5	83.5	31.361 a	17.491 a
	32.5	99.5	33.590 b	18.553 b

Means followed by different letters differ significantly by the Scott-Knott test at 5% probability.

The mean L* coordinate values obtained from natural immature coffee beans, according to storage time, are shown in Table 6, with an increase observed in the values of the coordinates analyzed with the extension of the storage time.

TABLE 6. Mean L* coordinate values for natural immature coffee beans subjected to different drying conditions and stored for 180 days.

Coffee type	Storage time (days)	L* coordinate
	0	29.244 a
Natural immature	60	32.657 b
	120	33.979 с
	180	34.533 c

Means followed by different letters differ by the Scott-Knott test at 5% probability.

Bleaching is a known phenomenon during the storage of processed coffee beans and is explained by the increase in the L* coordinate values. Increases in the a* and b* coordinates indicate the loss of the green and bluish colour of the beans, respectively (Afonso Júnior & Corrêa, 2003).

The colour of the natural immature coffee beans showed an increase in the L* coordinate value over the storage time and consequently experienced higher bleaching rates. This result for processed natural coffees, in addition to the bleaching factor, may be due to the presence of spermoderm (silver skin) fragments adhering to the beans, which may have influenced the reading of the apparatus (Abreu et al., 2015).

The percentages of black-green defective beans in the natural immature coffee sample, according to the relative humidity during drying, are shown in Table 7.

TABLE 7. Percentag	ge of black-green	defective beans	obtained after	drving of natu	ral immature coffee.
	8				

Relative humidity (%)	Black-green defective beans (%)	
10	33.00 ab	
17.5	37.00 b	
32.5	31.17 ab	

Means followed by the same letter do not differ by Tukey's test at 5% probability.

Black-green defective beans are characterized by a brilliant black colour because of the adherence of the silver skin. The immature and black-green coffee defects, originating from immature beans, are considered serious defects and negatively affect the quality of the coffee beverage (Brasil, 2003).

The data in Table 7 show that the mean number of defective beans varied among treatments, and for the coffees dried at a relative humidity of 32.5%, a lower percentage of black-green defectives beans was observed compared to the coffees dried at the relative humidity of 17.5%.

The drying temperature is another factor that affects the formation of black-green defective beans during this stage. Enzymes in the beans are thought to react with the substrate (phenolic compounds present near the cell wall), forming brown polymers. The same effect can also be produced by denaturation or oxidation of phenolic compounds, as well as of sugars and proteins (Teixeira et al., 1984).

CONCLUSIONS

Under the conditions tested in the present study, for the natural immature coffee, the Midilli model had the best fit for representing the drying kinetics, regardless of the relative humidity tested.

Regarding the physiological and physical quality of coffee, natural immature coffee had a better physical and physiological quality when dried at 32.5% relative humidity.

Drying with low relative humidities does not damage the physical and physiological quality of immature coffee immediately. The latent damage to quality was observed after 120 days of storage.

The mean number of defects varied among the treatments; in the coffees dried at 32.5% relative humidity, a lower percentage of black-green defective beans was observed compared to those dried at 17.5% relative humidity.

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